(15) SARDAR PATEL UNIVERSITY

## EXTERNAL EXAMINATION, APRIL 2014

M.Sc INDUSTRIAL CHEMISTRY-SEMESTER 2

## UNIT OPERATIONS II \& STOICHIOMETRY- PS02CICH01

$18^{\text {th }}$ April, 2015
Max.Marks:70
Time:10.30 a.m-1.30 p.m
Answer all the questions. Figures to the right side indicate marks

Q1.Write the number of the correct statement. All questions carry 1 mark each. (8*1=8marks)
a. In a shell \& tube heat exchanger,
i. square pitch gives more heat transfer area than triangular pitch.
ii. triangular pitch gives more heat transfer area than square pitch.
iii. both square \& triangular pitch give same heat transfer area
iv. cleaning facility is same in both square \& triangular pitch
b. Identify the correct relation.
i. $\quad 1 \mathrm{~W}=1 \mathrm{~J} / \mathrm{s}$ ii. $1 \mathrm{~W}=1 \mathrm{kcal} / \mathrm{s} \quad$ iii. $1 \mathrm{~W}=1 \mathrm{cal} / \mathrm{s} \quad$ iv. $1 \mathrm{~W}=1 \mathrm{cal} / \mathrm{hr}$
c. The -------------component is always present in less than its stoichiometric proportion with respect to other reacting components.
i.excess reactant ii.stoichiometric reactant iii. limiting reactant iv.none of these
d. Heat transfer occurs by natural convection because change in temperature causes difference in----
i. viscosity ii.thermal conductivity iii.heat capacity iv.density
e. Fouling factor of a heat exchanger depends on
i. length of fins ii.thickness of fins iii.scales formed iv.density of cold fluid
f. The overall resistance for heat transfer through a series of flat resistance is the ----- of the resistances
i. average ii. Product iii.geometric mean iv.sum
g. The temperature average used in heta exchanger calculation is -----temperature difference
i.arithmetic mean ii.geometric mean iii. Logarithmic mean iv. None of these
h. Multipass heat exchangers are used
i. Because of simplicity of fabrication
ii. For low heat load
iii. To obtain high heat transfer co-efficient \& shorter tube
iv. To reduce pressure drop

## Q2. Answer any seven ( each question carry two marks)

## (7*2=14 marks)

a. Define white body and opaque body
b. In which side (tube/shell) will you take viscous fluid in a shell \& tube exchanger? Justify your answer.
c. Distinguish between triangular and square pitch
d. Why are extended surfaces used in heat transfer?
e. Enlist the conditions when maximum heat transfer rate occurs in a heat exchanger
f. Define effectiveness of a heat exchanger
g. Define adiabatic flame temperature
h. Distinguish between sensible heat and latent heat
i. Define \% conversion and yield of reaction

Q3.
a.Discuss the significance of the following dimensionless numbers (06)

- Nusselts Number
- Grashoffs Number
- Prandtls Number
b. With the help of neat diagrams, distinguish between parallel and counter flow heat exchangers. (06) OR
b. Citing examples, distinguish between free and forced convection (06)


## Q4.

a. A fluid $(\mathrm{Cp}=4 \mathrm{~kJ} / \mathrm{kg} \mathrm{K})$ flowing at $23000 \mathrm{~kg} / \mathrm{hr}$ passes through a counter current heat exchanger at $130^{\circ} \mathrm{C}$. Water ( $\mathrm{C} \mathrm{p}=4.18 \mathrm{~kJ} / \mathrm{kg} \mathrm{K}$ ) flowing at $52000 \mathrm{~kg} / \mathrm{hr}$ and entering at $25^{\circ} \mathrm{C}$ is used to cool the fluid .If the heat transfer area is $11 \mathrm{~m}^{2}$ and the overall heat transfer co-efficient is $3500 \mathrm{~kJ} / \mathrm{hr} \mathrm{m}^{2} \mathrm{~K}$,find the exit temperatures of fluid and water using NTU method.
(06)
b. A multi pass Shell \& Tube heat exchanger is required to heat $25000 \mathrm{~kg} / \mathrm{hr}$ of cold water entering at $25^{\circ} \mathrm{C}$ using $20,000 \mathrm{~kg} / \mathrm{hr}$ of hot water entering at $100^{\circ} \mathrm{C}$ and leaving the exchanger at $80^{\circ} \mathrm{C}$. The cold water flow through 10 tubes each of OD 0.01 m and ID 0.008 m . The hot water flows through the annulus between tubes and a shell of dia 0.25 m . The thermal conductivity of the tube material is 60 $\mathrm{kJ} / \mathrm{hr} \mathrm{m} \mathrm{K}$. The properties of water are given below (06)
$\rho=1000 \mathrm{~kg} / \mathrm{m}^{3} \quad \mathrm{Cp}=4.18 \mathrm{~kJ} / \mathrm{kg} \mathrm{K} \quad \mu=3.6 \mathrm{~kg} / \mathrm{hrm} \quad \mathrm{k}=2.9 \mathrm{~kJ} / \mathrm{hr} \mathrm{mK}$
calculate the length of the heat exchanger if it is
A parallel exchanger
OR
A counter exchanger

## Q5.

a. Methane undergoes the following oxidation reactions.

$$
\begin{aligned}
& \mathrm{CH}_{4}+\mathrm{O}_{2}=\mathrm{HCHO}+\mathrm{H}_{2} \mathrm{O} \\
& \mathrm{CH}_{4}+2 \mathrm{O}_{2}=\mathrm{CO}_{2}+2 \mathrm{H}_{2} \mathrm{O}
\end{aligned}
$$

100 kmol of methane is charged to the reactor and the product stream contains 10 kmol Carbondioxide and 40 kmol formaldehyde. Calculate the \% conversion of methane and \% yield of formaldehyde.
b. 2000 kg of wet solids containing $70 \%$ solids by weight are fed to a tray drier where it is dried by hot air. The product obtained is found to contain $1 \%$ moisture by weight. Calculate (06)

- kg of water removed from wet solids
- kg of product obtained


## OR

b.An evaporator is fed with $15000 \mathrm{~kg} / \mathrm{h}$ of a solution containing $10 \% \mathrm{NaCl}, 15 \% \mathrm{NaOH}$ and rest water. During the process, water is evaporated and NaCl is precipitated as crystals. The thick liquor leaving the evaporator contains $45 \% \mathrm{NaOH}, 2 \% \mathrm{NaCl}$ and the rest water. Calculate (06)

- $\mathrm{kg} / \mathrm{h}$ of water evaporated
- $\mathrm{kg} / \mathrm{h}$ of salt precipitated
- $\mathrm{kg} / \mathrm{h}$ of thick liquor

Q6.
a. Calculate the heat to be transferred to a liquid stream of ethanol at its normal boiling point to generate $100 \mathrm{~kg} / \mathrm{h}$ of saturated ethanol vapour. $\lambda=842.3 \mathrm{~kJ} / \mathrm{kg}$
b. A stream flowing at the rate of $15 \mathrm{kmol} / \mathrm{h}$ containing $25 \% \mathrm{~N}_{2}$ and $75 \% \mathrm{H}_{2}$ is to be heated from 298 K to 473 K .Calculate the heat that must be transferred using the Cp data given below. (06)

| Gas | a | b | c | d |
| :--- | :--- | :--- | :--- | :--- |
| $\mathrm{N}_{2}$ | 29.59 | $-5.41^{*} 10^{-3}$ | $13.183^{*} 10^{-6}$ | $-4.97 * 10^{-9}$ |
| $\mathrm{H}_{2}$ | 28.61 | $1.019^{*} 10^{-3}$ | $-0.147^{*} 10^{-6}$ | $0.769^{*} 10^{-9}$ |

OR
b. Chlorine is manufactured using the reaction $4 \mathrm{HCl}+\mathrm{O}_{2} \rightarrow 2 \mathrm{Cl}_{2}+2 \mathrm{H}_{2} \mathrm{O}$ where $35 \%$ excess air is used.If the feed contains 4 kmol HCl and if the oxidation is $80 \%$ complete, calculate the heat that must be removed so that the products emerge at 600 K . The dry air and HCl enter at 560 K .
$\Delta H_{R}^{0}=-28600 \mathrm{~kJ} / \mathrm{mol}$
(06)

| $\mathrm{Cp}(\mathrm{KJ} / \mathrm{mol} \mathrm{K})$ | HCl | $\mathrm{O}_{2}$ | $\mathrm{~N}_{2}$ | $\mathrm{Cl}_{2}$ | $\mathrm{H}_{2} \mathrm{O}$ |
| :--- | :--- | :--- | :--- | :--- | :--- |
| $(560-298 \mathrm{~K})$ | 24.85 | 25.98 | 29.08 |  |  |
| $(600-298 \mathrm{~K})$ | 30.31 | 26.02 | 29.59 | 28.08 | 31.05 |

$-\times-$

